WO 2005/002711 PCT/EP2004/051345

- 7_i -

CLAIMS

1. Process to separate solids from a solids laden gaseous flow containing more than $100~\text{mg/Nm}^3$ solids by performing the following steps:

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- (a) separating solids from the gaseous flow using a gassolids separator resulting in a gaseous flow containing less than 50 mg/Nm³ solids and an underflow comprising the separated solids and part of the gaseous flow as fed to the gas-solids separator;
- (b) separating part of the solids from the underflow in a cyclone wherein solids and a gaseous flow containing still some solids are obtained; and
 - (c) contacting the gaseous flow obtained in step (b) with water to separate the solids and obtain a gaseous flow containing between 0 and 50 mg/Nm^3 solids; and
- (d) combining the gaseous flows which are poor in solids as obtained in step (c) and as obtained in step (a).
 - 2. Process according to claim 1, wherein the solids laden gaseous flow contains between 100 and 500 $\rm mg/Nm^3$.
 - 3. Process according to any one of claims 1-2, wherein the solids content in the gaseous flow as obtained in step (d) is between 10 and 50 mg/Nm^3 solids.
 - 4. Process according to any one of claims 1-3, wherein the gas-solids separator is a multi-separator vessel comprising of a plurality of parallel operated cyclonic gas-solids separators.
 - 5. Process according to any one of claims 1-4, wherein the ratio of mass of water to mass of gas contacted in step (c) is between 1.5 and 2.0.

WO 2005/002711 PCT/EP2004/051345

- 8 -

- 6. Process according to any one of claims 1-5, wherein the solids content in the gas after contacting with water in step (c) is smaller than 50 mg/Nm^3 .
- 7. Process according to claim 6, wherein the solids content in the gas after contacting with water in step (c) is between 0 to 5 mg/Nm^3 .

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- 8. Process according to any one of claims 1-7, wherein the gas flow containing less than 50 mg/Nm^3 solids as obtained in step (a) is fed to a gas expander turbine and wherein step (d) is performed downstream said gas expander turbine.
- 9. Process according to any one of claims 1-8, wherein the solids as obtained in step (b) are continuously fed to a collecting vessel, from which vessel the solids are discharged non-continuously to the environment via a lock-hopper vessel.